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A Subnanosecond Pulsed Electric Field System for Studying Cells Electropermeabilization

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Abstract—This article presents an experimental arrangement which, using 3-D numerical modeling, aims to study biomedical 2 effects using subnanosecond pulsed electric fields (PEFs). As part 3 of a major effort into developing contactless technology, the final 4 aim of this study is to determine conditions of the applied PEFs 5 (number of pulses, strength, pulse repetition frequency) able to produce electropermeabilization. The arrangement uses a pulsed power generator producing voltage impulses with an amplitude 8 of up to 20 kV on a 50- Ω matched load, with a rise time of 100 ps 9 and a duration of 600 ps. During the preliminary study reported 10 here, samples containing E. Coli were exposed to PEFs in a 11 4-mm standard electroporation cuvette, allowing the application 12 of a peak electric field strength of up to 60 kV/cm. The studies 13 were facilitated by detailed 3-D electromagnetic modeling of the 14 electric field distribution generated by voltage impulses inside the 15 system. Due to the nature of tests, the numerical analysis played 16 an essential role in the interpretation of results. Preliminary 17 biological results reported in this study are very encouraging, 18 showing that trains of 5000 to 50000 pulses applied at a pulsed 19 repetition frequency of 200 Hz (maximum PRF) can efficiently 20 induce E. Coli electropermeabilization. 21

Index Terms—Biological cells, electropermeabilization, pulsed
 electric fields (PEFs), pulsed power, subnanosecond pulses.

I. INTRODUCTION

THE use of narrow-band electromagnetic fields for application to medicine and biology has received significant attention by the scientific community over the last few decades [1]. Electroporation (electric pore formation) is a phenomenon which increases the permeability of the cell membrane when exposed to pulsed electric fields (PEFs) of high intensity

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and short duration. The pore formation generates openings in the cell membrane, allowing for the transfer of therapeutic molecules across the cell membrane [2], [3]. Thus, the electroporation phenomenon contributes to the efficiency of electrochemotherapy, when used with drugs [4] and electrogenetherapy, when used with DNA plasmids [5].

PEFs can cause reversible electroporation, i.e., a temporary permeabilization of the cell membrane [6], but they can also produce irreversible electroporation, i.e., cell death, for eradicating cancerous or other unwanted cells [7].

There are basically two types of PEF techniques applied *in vivo: invasive*, where metallic pairs of penetrating electrodes are used to apply the electric field and *noninvasive*, where the electric field is generated through electrodes brought in contact with the skin, without penetration of the body. In addition, the *contactless* term refers here to the approach dealing with the generation of electric fields remotely from the metallic structure of a *PEF source (antenna)*.

The *electrode-based contact* technology is already success-49 fully applied in the treatment of various cancers including, 50 but not limited to, kidney, liver, lung, and bone cancers [8]. 51 Pulses having hundreds of ns duration applied for cancer 52 treatment are still under clinical trials and as such are not part 53 of regular treatments. PEFs of about 100 μ s are widely used, 54 depending on the type and the evolution of cancer while ms 55 pulses are not used for cancer treatment. The outcome effect 56 depends not only on the magnitude and duration of the PEFs 57 delivered, but also on the pulse repetition frequency (PRF) 58 and on the characteristics of the tissue, in particular, its 59 conductivity. Irreversible electroporation using microsecond 60 very high intensity PEFs in the tissues is widely considered 61 in many hospitals. An advantage of this technique is that 62 the thermal effects are considerably lower, when compared 63 to other ablation techniques [9]. Cancer treatment techniques, 64 which include but are not limited to chemotherapy and surgery, 65 are unfortunately accompanied by adverse side effects imposed 66 on the patient [10], [11]. The future of the PEF-based cancer 67 treatment techniques is therefore closely related to the identi-68 fication of new ways to avoid the challenges imposed by the 69 existing *invasive* surgical procedures. The pathway toward a 70 *contactless* technology, a nonsurgical procedure, which aims at 71 overcoming some of the issues mentioned above, was studied 72 in very few research laboratories worldwide. The reason for 73 the very limited number of publications published in this 74 domain is perhaps due to the fact that, depending on their out-75 put voltage, the highly specialized HV subnanosecond pulsed 76

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power generators required are either extremely expensive or 77 only available at military related research centers. Even more 78 difficult, the focusing of electromagnetic radiation with very 79 high precision in a volume around 1 cm³, or preferably even 80 lower, is possible only using highly sophisticated impulse 81 antenna techniques. 82

Two possible solutions were suggested theoretically by Carl 83 Baum, as part of a major research effort undertook by the 84 Frank Reidy Research Center for Bioelectrics at Old Domin-85 ion University (USA): an impulse radiating antenna (IRA) 86 operated in air [12], [13], in combination with a complex 87 many layer dielectric lens [14] and another prolate-spheroidal 88 reflector, operated underwater [15]. More recently, at the same 89 research center, a dielectric rod antenna was also suggested 90 as a candidate for generating subnanosecond PEFs for the 91 stimulation of neurological tissue [16]. All the three tech-92 niques have been theoretically investigated using CST software 93 [15]–[17], with detailed numerical studies being reported. 94 In contrast, very limited experimental work has been pub-95 lished, and only using rather low voltage subnanosecond 96 pulsed power generators, with the resulting PEFs having 97 extremely low peak values when compared with the values 98 required for electroporation [18]-[20], the latter work rep-99 resenting an effort made at University of Limoges (France). 100 For stimulating deep inside a tissue, say at 8 cm [17] using 101 intense PEFs of some tens of kV/cm, published work suggest 102 a subnanosecond pulsed power generator with a peak output 103 voltage in excess of 250 kV is required [17]. Such a generator 104 is technically extremely challenging. 105

Another aspect is that when using such innovative contact-106 less delivery systems, the characteristics of the subnanosecond 107 PEFs are different when compared with those of the existing 108 PEF processing. A logical step is therefore to understand their 109 action on cells by firstly using standard electrode-based PEFs 110 driven by subnanosecond pulsed power generators. Results 111 published by the Old Dominion team and also by a research 112 group at Chongqing University (China), demonstrated that 113 subnanosecond PEFs can indeed produce: permeabilization 114 [21] followed by the transfer of molecules inside the cell [22], 115 cell stimulation with calcium mobilization (through VGCCs 116 activation) [23], and apoptosis (cell death) [24]-[27]. The main 117 issue with these results however is that they suggest a very 118 low efficiency of processing for a PEF having a relatively 119 low peak value, say around 25 kV/cm, as it is expected to 120 be generated in a deep tissue by a *contactless* reflector-based 121 system. Under such conditions, to obtain the effect on a 122 significant percentage of cells, it was necessary to apply an 123 extremely large number of pulses, of the order of a few 124 millions [22]. 125

The development of contactless PEF technologies has been 126 a major research theme in the long history of an ongo-127 ing collaboration between Pau University and Loughbor-128 ough University and two major works have been already 129 published discussing a novel technique for food process-130 ing [28] and a subnanosecond driven prolate antenna operated 131 underwater [29]. The latter work reports the first practi-132 cal demonstration of generating underwater a peak PEF 133 of 50 kV/cm at 8 cm away from any metallic structure, 134

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i.e., fulfilling the conditions required for *contactless* deep 135 tissue permeabilization [17].

The arrangement reported here is using a standard 137 electrode-based approach. In the preliminary phase of this 138 study, it was decided to apply PEFs on the E. Coli DH5 α 139 bacteria, which are very small cells with a diameter in the 140 range of 1 µm. 141

First, the pulsed power generator will be introduced, 142 together with its corresponding diagnostics. 143

Second, a detailed 3-D model is presented, based on the 144 CST Microwave Studio, a 3-D finite integral time-domain 145 (FITD) electromagnetic simulation software [30]. As the direct 146 measurement of the PEF generated inside a cuvette containing 147 the cell culture is technically challenging, a comprehensive 148 3-D modeling and numerical electromagnetic analysis were 149 essential during the experimental studies. 150

Third, we report encouraging preliminary results that 151 demonstrate that a high percentage of permeabilized bacteria 152 can be achieved using the described arrangement. 153

This conclusion ends with conclusions and a brief presen-154 tation of the way ahead. 155

II. EXPERIMENTAL ARRANGEMENT

For the present studies, a pulsed power generator similar to 157 that described in [31] was adapted for use as a subnanosecond 158 transient source capable of producing high voltage pulses 159 with an amplitude of up to 20 kV and having a 100-ps 160 rise time on a 50- Ω matched load, with a duration of about 161 600 ps. The generator is connected to the PEF processing 162 load through a 2.5-m-long RG214-U type coaxial 50- Ω cable, 163 having an insulator made of polyethylene with relative per-164 mittivity of 2.26. A simplified scheme of the pulsed power 165 arrangement is shown in Fig. 1. The generator is constructed 166 as a fast pulse forming line, with the closing switch operated 167 under high-pressure hydrogen. To obtain a 20-kV peak voltage 168 output, the product of the hydrogen pressure and the gap 169 distance of the electrode system was held to 22 bar · mm. 170 This value was then adjusted to obtain other values for the 171 output peak voltage. The output voltage is measured using a 172 capacitive voltage divider, the main voltage probe, attached 173 to the RG214-U coaxial cable [Fig. 1(b)]. The transmission 174 coefficient for this probe is equal to -46 dB all over the 175 frequency bandwidth and the reflection coefficient is lower 176 than -12 dB while the cut-off frequency is close to 6 GHz. 177

The PEF processing load connected at the end of 178 the RG214-U coaxial cable [Fig. 1(b)] consists of two 179 parallel-plate electrodes made of copper. The distance between 180 copper electrodes is fixed to 12 mm to allow mounting 181 between them a standard electroporation cuvette, having a gap 182 distance of 4 mm between its internal aluminum electrodes. 183 The volume of the sample which contains the deionized water 184 to be tested was kept at 100 μ L for two reasons. First, 185 to obtain the desired PEF in water in terms of amplitude, 186 rise time, and duration and second to reduce the impedance 187 mismatch. To avoid any possible electric breakdown, the upper 188 part of the cuvette was additionally filled with 1.6 mL of 189 paraffin oil, having a relative permittivity 2.33. It is important 190

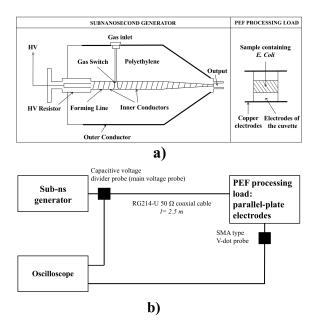


Fig. 1. Pulsed power arrangement for subnanosecond PEF. (a) Subnanosecond generator (adapted after [31]) and PEF processing load. (b) Overall schematic.



Fig. 2. Experimental arrangement for subnanosecond PEF processing. The numbers 1–6 represent the generator (1), capacitive voltage divider (main voltage probe) (2), RG214-U 50 Ω coaxial cable (3), two parallel-plate electrodes (4), 4-mm electroporation cuvette (5), and SMA-type V-dot probe (6).

to note that the dielectric strength of the present experimental 191 arrangement, when subnanosecond electric pulses are applied, 192 is much higher compared to cases when 50-Hz ac, microsec-193 ond or longer duration pulses are applied. The complete 194 experimental configuration is presented in Fig. 2. An SMA-195 type V-dot probe is mounted just a few millimeters below the 196 cuvette with the connector's body attached to the ground plate 197 electrode. This probe is used to control the voltage across the 198 cuvette, with the electric field in the cuvette obtained using 199 the numerical technique described in the following. 200

III. NUMERICAL TECHNIQUES

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A detailed 3-D modeling and EM analysis were carried out for the PEF system. To shorten the time required for numerical analysis of the 50- Ω (RG214-U) coaxial cable, only a length of 101 mm was considered, corresponding to a propagation time of 0.5 ns. The 3-D CST model of the

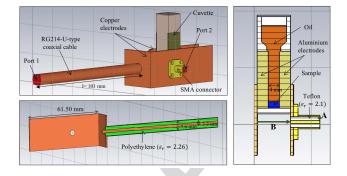


Fig. 3. Complete CST model for the PEF processing chamber, including the RG214-U coaxial cable, the two parallel-plate copper electrodes with the SMA-type V-dot probe attached and the electroporation cuvette, with various compartments filled with paraffin oil and water sample, which may contain bacteria. The two CST ports are highlighted.

PEF processing load is presented in Fig. 3. The presence of 207 bacteria in the water contained inside the cuvette was not taken 208 into consideration in the CST simulation, as measurements of 209 electrical permittivity and the real signals recorded from the 210 SMA-type V-dot probe, both demonstrated the bacteria do not 211 introduce a significant difference. To analyze the impedance 212 profile along the coaxial cable and in the PEF processing load 213 and to better understand its behavior due to the presence of 214 the electroporation cuvette, we have numerically performed the 215 time domain reflectometry (TDR) task in CST. The TDR was 216 evaluated based on the reflected signals using the integrated 217 Gaussian signal shown in Fig. 4, with a rise time of 219 ps and 218 a frequency bandwidth of 4 GHz, following the CST manual 219 formula [30]: 220

$$Z(t) = Z_0 \frac{\int_0^\infty i(\tau)d\tau + \int_0^t o(\tau)d\tau}{\int_0^\infty i(\tau)d\tau - \int_0^t o(\tau)d\tau}$$
(1) 22

where Z_0 is the characteristic impedance of the coaxial cable, 222 i.e., 50 Ω , i(t) is the incident signal at CST Port 1 (Fig. 3) 223 and o(t) is the reflected signal at the same port. Fig. 5 shows 224 the impedance is 50 Ω along the coaxial cable and then at 225 1 ns, which corresponds to the return end of the coaxial cable, 226 the impedance starts to increase to a value of 70 Ω . This 227 effect is due to the *mismatch* between the coaxial cable and 228 the PEF processing load. At around 1.2 ns the impedance 229 starts to decrease and at 1.4 ns attains a minimum value 230 of 32 Ω . This impedance decrease is due to the cuvette, 23 which is placed at a distance of 121 mm from the coaxial 232 cable input (Port 1). At around 1.8 ns the impedance again 233 increases rapidly this time due to the open end of the PEF load. 234 Both incident and reflected signals at Port 1 were carefully 235 analyzed to observe the impedance distribution within the 236 electric assembly. In addition, the estimation of the TDR 237 allows us to have a representation of the time variation of 238 the PEF processing load reflection coefficient (Fig. 6). 239

The electric field distribution inside the cuvette was studied using the CST Electrostatics solver. The cuvette behaves like a collection of two parallel plate capacitors mounted in parallel, one containing paraffin oil and the other water. Because of this, the electric field strength is the same in the two media, but the displacement fields are different. CST calculations indicate for

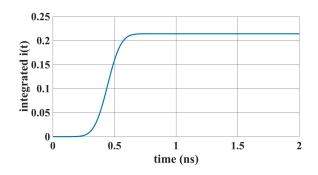


Fig. 4. Integrated Gaussian signal used to perform the TDR task.

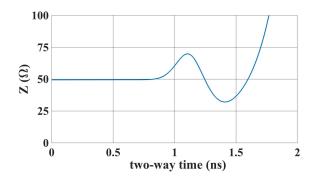


Fig. 5. Impedance profile along the cable and the processing load.

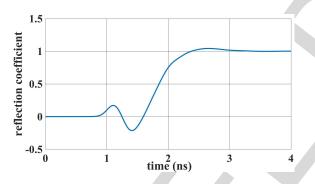


Fig. 6. Time variation of the reflection coefficient for the PEF processing load.

the cuvette a total equivalent capacitance of 5.95 pF, a value
allowing voltage pulses having about 258-ps rise time to be
delivered to the PEF processing load.

IV. DETERMINATION OF THE TIME VARIATION OF THE ELECTRIC FIELD IN THE PROCESSED WATER SAMPLE

Because of the very small size of the water sample to be 251 processed, there are no available techniques that can be used 252 to directly measure the electric field generated inside. The 253 only way to determine this essential parameter, which allows 254 the correct interpretation of the biological results, is to use 255 a combination of numerical modeling predictions and experi-256 mental evidence. Firstly, a detailed 3-D CST electromagnetic 257 analysis of the load was carried out, including the SMA-type 258 V-dot probe mounted near the cuvette (Fig. 7). The input 259 signal applied to the processing load (see Fig. 8) was accu-260 rately measured using the main voltage probe attached to the 261 RG214-U coaxial cable described above. This experimentally 262

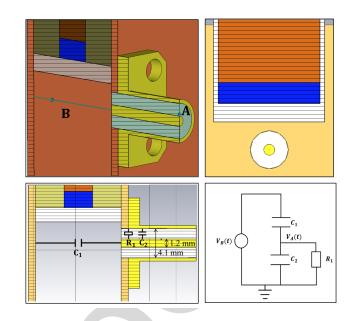


Fig. 7. Top: V-dot probe mounted inside the PEF load, near the cuvette containing the water to be processed. Bottom: its corresponding equivalent electric scheme, following that described in [32] and [33].

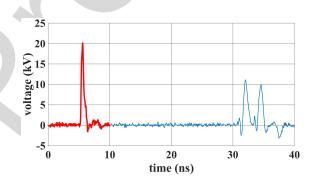


Fig. 8. Complete signal recorded from the main voltage probe considering the total length of 2.5 m for the RG214-U coaxial cable. The first 10 ns of the experimental voltage signal (highlighted) are used as CST input data.

obtained voltage signal, with a rise time of about 258 ps and 263 FWHM about 434 ps, was then used as an input (or excitation 264 signal) for the CST Port 1 situated at the coaxial cable input 265 (Fig. 3). To check the model, the predicted reflected signal was 266 then successfully compared with the experimentally recorded 267 reflected signal (see Fig. 9). To allow this comparison, the time 268 delay of the signal due to the 2.5-m coaxial cable (see Fig. 8) 269 was adjusted to the corresponding shorter time delay of only 270 101-mm length of cable considered by the CST model (see 271 Fig. 9). A second comparison between CST predictions and the 272 experimental data was performed for the CST Port 2 situated 273 at the V-dot probe output (Fig. 3). Fig. 10 demonstrates the 274 very good similarity between the predicted and the measured 275 signal. 276

The above presented preliminary work had two important consequences. 277

1) Following [32], the SMA-type V-dot probe could be calibrated, with the voltage V(t) calculated from the 280

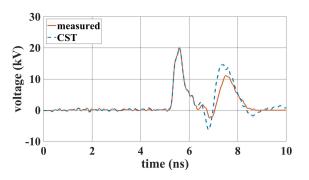


Fig. 9. Full line: experimental signal obtained from the main voltage probe. Dotted line: CST prediction for the voltage at Port 1.

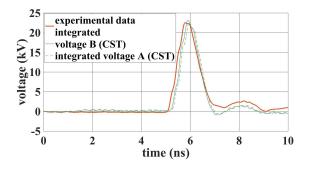


Fig. 10. Second comparison between CST model and experimental data. Thick line: time dependence of the integrated voltage signal from V-dot probe. Thin line: CST prediction obtained from a virtual voltage probe placed at location B. Dotted line: integrated voltage signal output from Port 2 placed at location A. The location of both A and B is presented in Fig. 7. The two CST generated traces are practically indistinguishable demonstrating that, due to the favorable electric field distribution, the SMA probe acts indeed as a V-dot probe [33].

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probe output voltage signal $V_{\text{signal}}(t)$ as:

$$V(t) = \frac{1}{\tau} \int_0^t V_{\text{signal}}(t) dt$$

(2)

where τ = Z₀ · C₁, with Z₀ = 50 Ω being the impedance of the cable connecting the probe to oscilloscope and C₁ = 2.9 fF the probe coupling capacitance [32], [33], as shown in Fig. 7 was obtained using CST calculations.
2) The following procedure was established. During testing, the electric field generated inside the water sample is calculated by CST, using an input voltage Port 1 based on the experimentally measured input voltage signal. However, as a precaution, the CST predictions for Port 2 are always checked against the experimental signal

generated by the V-dot probe housed inside the load.
 If the two are identical, the CST results are most likely
 correct. If the two are different, a possible explanation
 could be that electric breakdowns are present inside the
 processing load.

As an example, Fig. 11 presents the calculated time variation of the electric field strength inside the water sample for the experimental conditions of Fig. 9, i.e., when the peak transient voltage input reaches a peak of 20 kV. The corresponding peak electric field strength reaches 58 kV/cm, with a rise time of 303 ps and an FWHM of 773 ps. At this moment, the corresponding electric field distribution inside the processing load

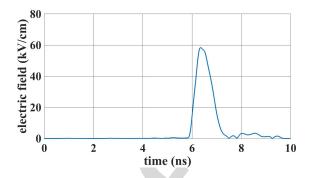


Fig. 11. PEF parameters generated inside the cuvette water sample, for the input conditions of Fig. 9. The peak electric field strength is reaching 58 kV/cm, with a rise time of 303 ps and a FWHM of 773 ps.

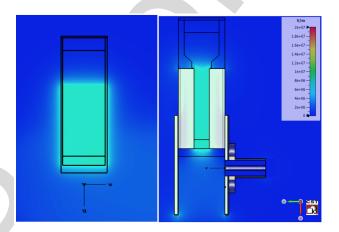


Fig. 12. Electric field distribution inside the processing load at the moment the peak field of 58 kV/cm is generated inside the cuvette water sample (see Fig. 11).

is shown in Fig. 12. It is important to note two essential characteristics: 1) the electric field is mainly concentrated inside the cuvette and 2) inside the cuvette the electric field is highly homogeneous, allowing a simple interpretation of the results obtained after PEF processing.

When performing a large number of tests at a high PRF, one important question is related to the possible temperature increase of the water sample. The variation of temperature ΔT during *N* consecutive shots is given by 311

$$\Delta T = \frac{W}{mC_p} N \tag{3} \quad 314$$

where *W* is energy deposited in the water during one shot, $m \approx$ 100 mg is the mass of the water sample and $C_p = 4188 \text{ J/kg/K}$ is the constant-pressure heat capacity of water at 25 °C [34]. The energy is calculated as

$$W = R \int_0^t I^2(t') dt'$$
 (4) 319

where *R* is the water sample resistance while the current integral was performed using data from a CST virtual current sensor. As the water sample has a conductivity of about $\sigma = 300 \ \mu$ S/m and a relative permittivity $\varepsilon_r = 78.4$ at 25 °C [35], the time constant $\varepsilon_0 \varepsilon_r / \sigma = 140 \ \mu$ s is much larger than the pulse duration (≈ 2 ns) and therefore the conduction 325

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current can safely be ignored. In such conditions the water series equivalent resistance can be estimated as

$$R = \frac{\tan \delta}{2\pi f C_w} = 1.28 \ \Omega \tag{5}$$

where $\tan \delta = 0.005$ [35] is the water loss tangent at a frequency *f* estimated as $f = 0.35/t_{rise} = 1.35$ GHz, where $t_{rise} = 258$ ps is the rise time of the impulse. The equivalent capacitance C_w of the water sample was calculated using CST as $C_w = 4.6$ pF. As a typical result, after applying $N = 50\,000$ consecutive shots, the estimated water sample temperature increase is only $\Delta T = 0.00615^{\circ}$ C and therefore negligible.

V. BIOLOGICAL TECHNIQUES

DH5a were purchased Е. Coli from Invitrogen 337 (Courtaboeuf, France). Cultures used for experiments 338 were grown from 80 μ L of bacterial stock solution (saturated 339 bacterial broth mixed with glycerol in (1:1) ratio stored at 340 -80 °C) added to 8 mL of Luria Bertani (LB) medium 341 (Invitrogen LB broth base Lennox L) and incubated at 37 °C 342 under constant orbital shaking at 220 r/min for 8 h over day, 343 corresponding to an endpoint OD600 of approximately 0.9. 344 Cultures were then placed at 4 °C overnight until used for 345 experiments on the next day. E. Coli permeabilization was 346 assessed using a cell-impermeant fluorescent nucleic acid 347 stain entering only permeabilized bacteria, the YO-PRO-1 348 iodide (λ_{ex} 491/ λ_{em} 509) (Invitrogen). E. Coli gating in flow 349 cytometry was validated using a cell-permeant fluorescent 350 nucleic acid stain entering all bacteria, permeabilized or not, 351 the SYTO 9 (λ_{ex} 485/ λ_{em} 498) (Invitrogen). Prior to PEF 352 exposure, bacteria were centrifuged at $2000 \times g$ for 20 min, 353 the supernatant was discarded and the bacterial pellet was 354 resuspended in the same volume of sterile deionized water 355 (same bacterial concentration than mother culture). Then, 356 either YO-PRO-1 iodide or SYTO 9 was added (working 357 concentrations of 30 and 50 μ M, respectively). A volume 358 of 100 μ L of bacterial suspension with marker (YO-PRO-1 359 iodide or SYTO 9) was then placed in a 4-mm wide gap 360 commercial electroporation cuvette (Cell Projects Ltd, Kent, 361 U.K.) and covered with 1.6 mL of insulating paraffin oil 362 in order to prevent arcing between electrodes during PEF 363 exposure. Then, pulses were delivered at room temperature 364 by installing the electroporation cuvette in the applicator 365 presented in Fig. 3. Controls were sham exposures for which 366 all the steps of the exposure protocol were followed, except 367 for the PEF delivery. 5 min after PEF exposure, a volume 368 of 50 μ L of the bacterial suspension was collected from 369 the cuvette and mixed with 50 μ L of sterile deionized 370 water. On average 30 min after PEF exposure, and prior 371 to flow cytometry analyses, this bacterial suspension was 372

TABLE I

RESULTS FROM PERMEABILIZATION EFFECT FOR VARIOUS NUMBER OF PULSES APPLIED WHEN AN ELECTRIC FIELD OF 58 kV/Cm WAS APPLIED AT 200-Hz PRF

Number of pulses applied	Percentage of permeabilized bacteria (mean ± standard deviation)	Number of replicates*
5000	44.4 ± 9.3	3
10000	69.4 ± 12.3	6
25000	81.0 ± 7.4	6
50000	89.3 ± 4.7	6

* The « number of replicates » is the number of times a given condition was tested on bacteria coming from different independant bacterial cultures.

mixed with 600 μ L of LB medium. Flow cytometry analyses 373 were performed using a BD Accuri C6 Flow Cytometer 374 (Bd Biosciences, le Pont-de-Claix, France). An excitation 375 laser of 488 nm and the FL1 bandpass filter 533/30 were 376 used to detect fluorescence of either YO-PRO-1 iodide and 377 SYTO 9 (the reason why these markers could not be used 378 simultaneously). For data processing, E. Coli were gated 379 and separated from debris based on FSC-A and SSC-A 380 morphological criteria. Nevertheless, a small proportion of 381 events was not SYTO 9 positive within this gating, meaning 382 that there was still debris. Thus, the specificity of the gating 383 was calculated as (6) and (7), shown at the bottom of the 384 page. 385

The specificity of the gating was evaluated for the different experimental conditions (Sham or PEF exposures), and was considered for further data processing. Finally, the percentage of permeabilized bacteria was calculated using YO-PRO-1 iodide following (7).

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VI. PRELIMINARY RESULTS

We assessed the ability of the subnanosecond pulses deliv-392 ered by our system to induce electroporation on E. Coli DH5 α , 393 applying trains of 5000 to 50000 pulses at a PRF of 200 Hz 394 at an electric field amplitude of 58 kV/cm (the top electric 395 field amplitude deliverable with the present arrangement). All 396 conditions tested efficiently generated electroporation of the 397 bacteria to YO-PRO-1 iodide, a fluorescent nucleic acid stain 398 and cell permeabilization marker of approximately 630 Da. 399 Moreover, under these conditions, we observed an additive 400 effect of the pulses, the percentage of permeabilized bacteria 401 increasing from 44.4 % \pm 9.3 % to 89.3 % \pm 4.7 % for 5000 to 402 50000 pulses applied, respectively (Table I). Importantly, 403 no increase of the temperature within the samples submitted to 404 PEF treatment was noticed under the conditions tested in this 405 study, in line with the estimated temperature rise presented 406 above under Section IV. Thus, the permeabilization of E. Coli 407 observed in response to PEF exposure performed in this study 408 cannot be attributed to thermal effects. 409

Gating Specificity (GS) =	number of SYTO®9 positive events			(6)
	total number of events			(0)
% permeabilized bacteria =	% of YO-PRO-1 positive events in sample	% of YO-PRO-1 positive events in control GS control	<u>1</u> - × 100	(7)
	$100 - \frac{\% \text{ of YO-PRO} - 1 \text{ positive events in control}}{\text{GS control}}$		X 100	()

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VII. CONCLUSION AND THE WAY AHEAD

A relatively simple arrangement for PEF processing driven 411 by a subnanosecond pulsed power generator has been devel-412 oped and tested. The preliminary results show that sub-413 nanosecond processing can be highly efficient. The way ahead 414 will require the development of a compact, high PRF and 415 mobile subnanosecond 0.5-MV pulsed power generator that, 416 when coupled with a prolate reflector, will allow biomedical 417 experimentation at (or near) a hospital. 418

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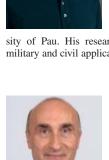
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